## Na<sub>2</sub>ZrO<sub>3</sub> Stability under Reforming/Regeneration Cycles during the Steam Reforming of Ethanol with CO<sub>2</sub> Absorption

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## ABSTRACT

In this work Na<sub>2</sub>ZrO<sub>3</sub> and a Ni-Al<sub>2</sub>O<sub>3</sub> catalyst were used to evaluate the hydrogen production by the steam reforming of ethanol in combination with CO<sub>2</sub> absorption. The Na<sub>2</sub>ZrO<sub>3</sub> was synthesized by the solid state method with a Na<sub>2</sub>CO<sub>3</sub>/ZrO<sub>2</sub> = 1:1 molar ratio and calcined at 900 °C in air. A 25% W Ni-Al<sub>2</sub>O<sub>3</sub> catalyst was synthesized by incipient impregnation and calcined at 900 °C in air. During reforming, operating conditions were:  $H_2O/C_2H_5OH = 6:1$  molar ratio, T = 600 °C, SV = 414 h<sup>-1</sup>, with a reactor loading of Ni-Al<sub>2</sub>O<sub>3</sub>/Na<sub>2</sub>ZrO<sub>3</sub> = 0.2g/3.7g. Results of the X-ray absorbent confirmed the Na<sub>2</sub>ZrO<sub>3</sub> crystalline phase. While, the catalyst shown NiO and Al<sub>2</sub>O<sub>3</sub> phases with a surface area of 125 m<sup>2</sup>/g. TGA CO<sub>2</sub> absorption tests by Na<sub>2</sub>ZrO<sub>3</sub> reached 84.3% of the theoretical absorption value. Ethanol steam reforming without absorbent reached a maximum concentration of 69.1% H<sub>2</sub> (dry basis). After reaction X-ray results shows Ni and Al<sub>2</sub>O<sub>3</sub> phases, while maintaining its initial surface area. Regeneration of the absorbent was carried out by separating this from the catalyst followed by calcination in air at T = 900 ° C by 4 hours. For the following reaction cycle the regenerated absorbent was remixed with the catalyst and reloaded to the reactor for a new step of reforming completing a reforming-regeneration cycle (R-Reg). 10 R-Reg cycles were performed resulting an excellent thermal and chemical stability of the Na<sub>2</sub>ZrO<sub>3</sub> absorbent. While, during the reforming step an average of 92% H<sub>2</sub> (dry basis), together with 8% CO<sub>2</sub>, and CO free with an absorbent carbonation of 17.7% W. These observed values are close to the thermodynamic equilibrium and show excellent compatibility between the reforming and carbonation kinetics, and a great thermal stability of materials resulting in an attractive process for hydrogen production

Keywords: Absorption enhanced reforming; Na2ZrO3; Reforming/regeneration cycles







